# **TRANSPORT PHENOMENA (CHEN 4101)**

**Time Allotted : 3 hrs** Full Marks : 70

*Figures out of the right margin indicate full marks.*

*Candidates are required to answer Group A and any 5 (five) from Group B to E, taking at least one from each group.*

*Candidates are required to give answer in their own words as far as practicable.*

# **Group – A (Multiple Choice Type Questions)**

- 1. Choose the correct alternative for the following:  $10 \times 1 = 10$ 
	- (i) For an unit vector  $\delta_1$  along x-direction and  $\delta_2$  along y-direction the definition for unit dyad δ1δ<sup>2</sup> yields \_



(ii) Using Von-Karman integral method the thickness of momentum boundary layer is equal to \_\_\_\_\_\_\_\_\_

(a) x 4.64 Re (b) x 2.32 Re (c) x 1 Re (d) x 9.28 Re

(iii)  $\vec{\nabla} \times (c\vec{U}) =$  $\rightarrow$  (  $\rightarrow$ \_\_\_\_\_\_\_\_\_\_\_\_\_, where 'c' is the constant (a)  $c\vec{v} \times \vec{U}$ (b)  $c\vec{v} \cdot \vec{U}$ (c)  $c \times (\vec{\nabla} \times \vec{U})$  $\ddot{\phantom{0}}$ (d)  $c \times (\vec{\nabla} \cdot \vec{U})$  $\frac{1}{2}$   $\frac{1}{2}$ 

(iv) In the modified Reynolds analogy the 'j' factor for mass transfer is equal to (a)  $St_m Sc^{1/3}$  (b)  $St_HSc^{1/3}$  $(c)$  St<sub>m</sub>Sc<sup>2/3</sup>  $(d)$  St<sub>H</sub>Sc<sup>2/3</sup>.

(v) For fluctuating properties  $\phi_1$  and  $\phi_2$ , the time averaging of the product of these properties yields \_\_\_\_\_\_\_\_\_\_\_\_\_\_

(a)  $\phi_1^{\text{mean}} \phi_2^{\text{mean}} + \phi_1 \phi_2^{\text{'}}$  (b)  $\phi_1^{\text{mean}} \phi_2^{\text{mean}}$ (b)  $\phi_1^{\text{mean}} \phi_2^{\text{mean}}$ (c)  $\phi_1 \phi_2$  $\phi_1 \phi_2$  (d)  $\phi_1^{\text{mean}} \phi_2^{\text{mean}} + \phi_1 \phi_2$ 

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- (vi) Turbulent energy dissipation function is dependent on \_\_\_\_\_\_\_\_
	- (a) gradient of the temperature fluctuation
	- (b) gradient of the velocity fluctuation
	- (c) product of gradient of velocity fluctuation
	- (d) none of above.

(vii) The radius of a capillary tube (length: 0.5 m) is equal to \_\_\_\_\_\_\_\_\_ for a Newtonian liquid (density: 955.2 kg/m<sup>3</sup>; kinematic viscosity:  $4.03 \times 10^{-5}$  m<sup>2</sup>/s) flow with mass flow rate of 0.003 kg/s. Pressure drop in the tube: 4.829 x 10<sup>5</sup> Pa. (a)  $7.51 \times 10^{-4}$  m (b)  $8.51 \times 10^{-4}$  m (c)  $9.51 \times 10^{-4}$  m (d)  $10.51 \times 10^{-4}$  m.

(viii) When vapor condenses on a cooled wall the thickness of the resulting liquid film  $is$ 

(a) directly proportional to the latent heat of condensation of the vapour

- (b) inversely proportional to the latent heat of condensation of the vapor
- (c) has no relation to latent heat of condensation of the vapour
- (d) directly proportional to the square of latent heat of condensation of the vapour.
- (ix) The Lennard-Jones potential function is given by \_\_\_\_\_\_\_\_\_\_\_\_\_\_\_\_\_, where r is the actual distance between a pair of molecules,  $\sigma$  is the collision diameter and  $\varepsilon$  is the characteristic energy of the molecules.

(a) 
$$
4\varepsilon \left[ \left( \frac{\sigma}{r} \right)^6 - \left( \frac{\sigma}{r} \right)^{12} \right]
$$
  
\n(b)  $4\varepsilon \left[ \left( \frac{\sigma}{r} \right)^{12} - \left( \frac{\sigma}{r} \right)^6 \right]$   
\n(c)  $4\varepsilon \left[ \left( \frac{\sigma}{r} \right)^3 - \left( \frac{\sigma}{r} \right)^{12} \right]$   
\n(d)  $4\varepsilon \left[ \left( \frac{\sigma}{r} \right)^{12} - \left( \frac{\sigma}{r} \right)^3 \right]$ 

- (x) For fluids with Pr  $>1$ , the temperature boundary layer
	- (a) overlaps with velocity boundary layer
	- (b) lies outside the velocity boundary layer
	- (c) lies inside the velocity boundary layer
	- (d) overlaps with the velocity boundary layer.

### **Group – B**

- 2. (a) For an irrotational two dimensional flow of a fluid (density  $\rho$ ) show that the value of the exponent m is equal to either 0 or 1, when  $u_x(x,y) = Cx^m$ ,  $u_y(x,0) = 0$ and  $P(0,0)=P_0$ .  $u_x$  is the x direction component of velocity u,  $u_y$  is the y direction component of velocity u and P is the applied pressure to generate flow.
	- (b) "No-slip assumption's validity during the formulation of any transport model for a fluid flow inside a conduit depends on the geometry of the conduit." – Justify the appropriateness of the statement.

### **9 + 3 = 12**

3. (a) "In a cartesian coordinate system a scalar, vector and tensor can be represented with 3<sup>0</sup>, 3<sup>1</sup> and 3<sup>2</sup> respectively." – Justify the correctness of the statement.

(b) The following data are available for the viscosities of mixtures of hydrogen and Freon-12 (dichlorodifluoromethane) (MW 120.92) at 25°C and 1 atm:



Find out the viscosity of the mixture, when 50% of hydrogen is mixed with 50% of Freon-12.  $3 + 9 = 12$ 

#### **Group – C**

- 4. (a) Applying shell momentum balance, derive Hagen-Poiseuille equation in case of a laminar flow of an incompressible Newtonian fluid in a circular tube.
	- (b) "The logic behind Reynold's analogy is the similarity between nondimensional form of the convection-diffusion equation for any transport process, when both Pr=1 and Sc=1." – Prove the correctness of the statement.

 $7 + 5 = 12$ 

- 5. (a) For the turbulent flow in smooth circular tubes, the function  $\frac{\overline{V}_z}{\overline{V}_{z,\text{max}}} = \left(1 \frac{r}{R}\right)^{r}$  $\left(1-\frac{r}{n}\right)^{\frac{1}{n}}$ z,max  $\frac{\nabla_z}{\nabla_z} = \left(1 - \frac{r}{R}\right)$  $\overline{\mathsf{v}}_{_{\mathsf{z}\,\mathsf{max}}}$  ( R is sometimes useful for curve-fitting purposes: near  $Re=4 \times 10^3$ , n=6; near  $Re=1.1$  $\times$  10<sup>5</sup>, n=7; and near Re=3  $\times$  10<sup>6</sup>, n=10. Show that the ratio of average to maximum velocity is  $\frac{\sqrt{v_z}}{\overline{v}_{z,\text{max}}} = \frac{2H}{(n+1)(2n+1)}$  $+1)(2n+1$  $\langle z \rangle$  2n<sup>2</sup> z,max  $\overline{\mathsf{v}}_{\mathsf{z}}\rangle$  2n  $\bar{v}_{z_{\text{max}}}$   $(n+1)(2n+1)$ .
	- (b) Show that the time averaging of the product of two properties  $\phi_1$  and  $\phi_2$  is given by  $\phi_1\phi_2=\Phi_1\Phi_2+\phi_1\phi_2$  , where  $\Phi$  is the mean component and  $\phi'$  is the fluctuating component of  $\phi$ .  $7 + 5 = 12$

# **Group – D**

6. (a) Fig. 1 given below shows heat conduction in a finite slab of given dimensions. The thermal conductivity and density of the slab are 0.96 cal/(cm s  $\degree$ C) and 8 gm/cc. The slab is initially kept at 20 °C.





State the governing equation together with all boundary and initial conditions. Derive the dimensionless form of all equations. Show detailed steps.

(b) Derive the equation for temperature profile as a function of time and space. You are required to determine the temperature profile along the slab at 10s.

 $4 + 8 = 12$ 

7. Calculate the thermal conductivity of a mixture containing 10 mole  $% CO<sub>2</sub>$  and 50 mole % H<sup>2</sup> and the rest Ar at 1 atm and 300K**.** The following data is given:



#### **Group – E**

8. Cl<sub>2</sub> (A)-air mixture is fed to a chamber filled with cyclohexene  $(C_6H_{10})$  dissolved in CCl<sub>4</sub>. It was found that the reaction of  $Cl_2$  with  $C_6H_{10}$  is second order with respect to  $Cl_2$  and zero order with respect to  $C_6H_{10}$ . Hence the rate of disappearance of  $Cl_2$  per unit volume is  $k_2C_A^2$ . B is a  $C_6H_{10}$  - CCI<sub>4</sub>, mixture, assuming that the diffusion can be treated as pseudobinary. Assume that the air is essentially insoluble in the  $C_6H_{10}$  - CCl<sub>4</sub>, mixture. Let the liquid phase be sufficiently deep that L can be taken to be infinite. Show that the

concentration profile is given by  $\frac{C_{A0}}{C} = \left(1 + \sqrt{\frac{k_2 C_{A0}}{C}} \right)^2$  $\left(\begin{array}{cc} \sqrt{6} & \sqrt{6} \\ \sqrt{6} & \$ 2 A0 \_| 1 \_ | 12 A0 A (V<sup>JL</sup>AB  $\frac{C_{A0}}{2} = \frac{1}{1 + \frac{1}{1 + \frac{1}{1}} \cdot \frac{1}{1 + \frac{1}{1}} \cdot \frac{1}{1}}$  $C_{\rm A}$  (  $\sqrt[3]{6}$ D

Explain the significance of Reynolds analogy in transportation of a quantity during fluid flow?

#### **9 + 3 = 12**

9. (a) A droplet of liquid A, of radius  $r_1$  is suspended in a stream of gas B. We postulate that there is a spherical stagnant gas film of radius  $r_2$  surrounding the droplet. The concentration of A in the gas phase is  $x_{A1}$  at  $r = r_1$  and  $X_{A2}$  at the outer edge of the film,  $r = r_2$ . By a shell balance, show that for steady-state diffusion  $r^2N_{Ar}$  is a constant within the gas film, and set the constant equal to  $r_i^2N_{\text{Arr}}$  at the droplet surface also show that the result leads to the following equation for  $x_A$ .

$$
r_1^2 N_{A r 1} = -\frac{c D_{AB}}{1 - x_A} r^2 \frac{dx_A}{dr}
$$

(b) What is the purpose of calculating mass transfer average velocity in two different ways – one is the mass average velocity and the other one is the molar average velocity?

 $9 + 3 = 12$ 

