B.TECH/CHE/4TH SEM/CHEN 2201/2021

HEAT TRANSFER (CHEN 2201)

Time Allotted : 3 hrs

Full Marks: 70

 $10 \times 1 = 10$

Figures out of the right margin indicate full marks.

Candidates are required to answer Group A and <u>any 5 (five)</u> from Group B to E, taking <u>at least one</u> from each group.

Candidates are required to give answer in their own words as far as practicable.

Group – A (Multiple Choice Type Questions)

- 1. Choose the correct alternative for the following:
 - (i) Thermal resistance of composite wall is maximum when slabs of different materials are arranged in

 (a) Parallel
 (b) partly parallel & partly series
 - (d) Series
 - (c) random

(ii) An increase in fin effectiveness is caused by high value of (a) convective coefficient (b) thermal conductivity (c) cross-section area (d) circumference

- (iii) Drop wise condensation takes place on
 (a) smooth surface
 (b) rough and contaminated surface
 (c) gray surface
 (d) none of these
- (iv) Lieden-frost effect is associated with
 (a) evaporation of a solution
 (b) boiling liquid on a hot surface
 (c) exchange of heat between two fluids
 (d) condensation of vapour on a cold surface
- (v) Reynolds analogy states that (a) $S_t = f/2$ (b) $S_t = f/4$ (c) $S_t = 4f$ (d) $S_t = \sqrt{f}$

(vii) The Sieder and Tate equation is used for the determination of heat transfer coefficient of fluid

- (a) Flows through a circular tube when flow is laminar
- (b) Flows through a circular tube when flow is turbulent
- (c) Flows over a flat plate when flow is laminar
- (d) Flows over a flat plate when flow is turbulent

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- (viii) Thermal boundary layer is almost equal to hydrodynamic boundary layer for(a) Gas(b) Solid
 - (c) Liquid metal (d) Oil
- (ix) The rate of heat transfer between two large parallel planes with one radiation shield is(a) Double
 - (b) Half
 - (c) Equal
 - (d) Logarithmic value of the radiation heat transfer between them in absence of radiation shield
- (x) For a 2-4 exchanger where steam is condensing outside the tubes, the value of LMTD correction factor is
 - (a) 0

(c) 1

(b) 0.5(d) Infinity

Group – B

- 2. (a) Derive a governing differential equation for steady state radial heat conduction with uniform heat generation in a cylindrical body.
 - (b) Show that in a long cylinder of radius R with uniformly distributed heat source, the temperature distribution is prescribed by the relation $\frac{T - T_w}{T_{max} - T_w} = 1 - \left(\frac{r}{R}\right)^2$ where, T_w is the temperature at the outer surface of the cylinder and T_{max} is the

maximum temperature in the cylinder.

5 + 7 = 12

- 3. (a) Define fin efficiency for heat transfer from extended surface. Determine an expression for the efficiency of a finite length fin having its tip perfectly insulated.
 - (b) During a heat treatment process, alloy steel spherical ball of 12mm diameter are initially heated to 800°C in a furnace. Subsequently, these are cooled in an oil bath at 35°C with convective coefficient 20 W/m²-K. Determine the time required for the cooling process. Also calculate the convective coefficient if it is desired to complete the cooling process in 10 minutes. The thermo-physical properties of steel ball are: Density 7750 kg/m³; specific heat 520 J/kg-K; conductivity 50 W/m-K.

(2+4)+6=12

Group – C

- 4. (a) Derive the Reynold's analogy.
 - (b) Hot air flows with a mass rate of 0.050 kg/s through an uninsulated sheet metal duct of diameter of 0.25m. The hot air enters at 120°C and after a distance of 5 m, cools to 77°C. The heat transfer coefficient between the duct outer surface

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and the ambient air at 0°C is known to be outer heat transfer coefficient is 6 W/m²k. Determine the heat flux and the duct surface temperature at x = L. Air properties at 363K, $C_p = 1010 \text{ J/kg-K}$ at 350K, k =0.030 W/m-K, $\mu = 208.2 \times 10^{-7} \text{ N-s/m}^2$, Pr = 0.70

6 + 6 = 12

- 5. (a) Write a short note on thermal boundary layer.
 - (b) Determine the average convection heat transfer coefficient for the 2.5-m-high vertical walls of a home having respective interior air and wall surface temperatures of (a) 20 and 10°C and (b) 27 and 37°C. Thermo-physical properties of Air at 288K, 1 atm are, $\beta = 1/T_f = 3.472 \times 10^{-3} \text{ K}^{-1}$, $\nu = 14.82 \times 10^{-6} \text{ m}^2/\text{s}$, k = 0.0253 W/m-K, $\alpha = 20.9 \times 10^{-6} \text{ m}^2/\text{s}$, Pr = 0.710Thermo-physical properties of Air at 305K, 1 atm are, $\beta = 1/T_f = 3.279 \times 10^{-3} \text{ K}^{-1}$, $\nu = 16.39 \times 10^{-6} \text{ m}^2/\text{s}$, k = 0.0267 W/m-K, $\alpha = 23.2 \times 10^{-6} \text{ m}^2/\text{s}$, Pr = 0.706. (Symbols bear usual significance).

4 + (4 + 4) = 12

Group – D

- 6. (a) Discuss the detail the various regimes in pool boiling and explain the condition for the growth of bubbles. What is the effect of bubble size on boiling
 - (b) Saturated steam at atmospheric pressure condenses on the outer surface of vertical tube of length 1 m and outer diameter 75 mm. the tube wall is maintained at a uniform surface temperature of 40°C by the flow of cooling water inside the tube. Estimate the steam condensation rate and the heat transfer rate to the tube. What water flow rate will result in a 5°C temperature difference between the outlet and inlet of the pipe? Also calculate the flow Reynolds number to check the assumption of laminar flow conditions. Given, the thermo-physical properties of saturated water are as follows: latent heat of vaporization = 2258.76 kJ/kg; density = 977.8 kg/m³; thermal conductivity = 2.403 kJ/m-hr-K; viscosity = 4.06×10⁻⁴ kg/m-s.

(4+2)+6=12

- 7. (a) State Kirchhoff's law. What is radiation shield?
 - (b) (i) Calculate the net radiant heat exchange per m^2 area for two large parallel planes at temperatures of 427°C and 27°C respectively. ϵ (hot plane) = 0.9 and (cold plane) = 0.6.
 - (ii) If an aluminum shield ($\epsilon = 0.04$) is placed between them, find the percentage reduction in the heat transfer.

(2+2)+8=12

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- 8. (a) Describe the 2-4 pass heat exchanger with the help of schematic diagram. What is LMTD correction factor?
 - (b) What are the main functions of baffles in a shell and tube exchanger? Draw the temperature profile of a parallel flow and counter flow for different heat capacity rate of fluid.

(3+3) + (3+3) = 12

- 9. (a) (i) How can you explain the increase in steam economy for a multiple effect evaporator as compared to a single effect evaporator?
 - (ii) When is backward feed mode of operation more suitable than forward feed mode for a multiple effect evaporator? Explain.
 - (b) A triple effect forward feed evaporator is used to concentrate a liquid which has marginal elevation in boiling point. The temperature of the stream to the first effect is 105°C, and the boiling point of the solution within third effect is 45°C. The overall heat transfer coefficients are 2200 W/m², 1800 W/m² and 1500 W/m² in the I-effect, II-effect and III-effect respectively. Find out at what temperatures the fluid boils in the I and II effects.

(3+3)+6=12

| Department & Section | Submission Link |
|-------------------------|--|
| CHE(Regular) | https://classroom.google.com/c/MzEyNTM2NjA2MzU1/a/MzcxNjU1NzIwNTUw/details |
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