

### B.TECH/CHE/3rd SEM /CHEN 2104/2015 2015

#### Industrial Stoichiometry (CHEN 2104)

Full Marks : 70

Allotted : 3 hrs

Figures out of the right margin indicate full marks.

Candidates are required to answer Group A and any 5 (five) from Group B to E, taking at least one from each group.

didates are required to give answer in their own words as far as practicable.

Group - A (Multiple Choice Type Questions) 10 x 1=10 oose the correct alternatives for the following: A gas mixture contains 28 kg N<sub>2</sub>, 16 kg  $O_2$  and 17 kg NH<sub>3</sub>. The volume fraction of wgen in the mixture is: d) 0.25. c) 0.355 b) 0.20 0.262 for the equation D(m) = a t(s) + b, the units of a are d) none of the above. c)s/m b)m/s Air contains 21 mol%  $O_2$  (mol. wt. = 32) and 79 mol%  $N_2$  (mol. wt = 28). The average olecular weight of air is: d) 27.50. c) 25.24 b) 28 29

Clausius – Clapeyron equation is valid when heat of vaporization of a substance: b) is dependent on temperature a) is independent of temperature d) is dependent on pressure. c) is independent of pressure

of the solvent Addition of a non-volatile solute to a solvent results in \_ b) boiling point depression a) freezing point elevation c) vapour pressure lowering

1

d) none of these.

The reference temperature during enthalpy calculation a) must be same for all the streams of the plant b) may not be same for all the streams of the plant c) is always taken as 298 K d) none of the above.

<sup>[]</sup> <sup>0</sup>API is given by (a) <u>141.5</u>-131.5 (c)  $\frac{G}{141.5}$  - 131.5

EN 2104

(b)  $\frac{131.5}{G}$  - 141.5 (d) none of the above. **F TECHN** 

**TARY BIC** 

6610199

as far as pr

·e

HE/Odd/Sem-3		
	B.TECH/CHE/3rd SEM (CUEN DAD IN	
	(viii) The negative of the state of the stat	
late the standa	combustion product is known as:	
$_{2\Pi_{5}OH(1)} + O$	a) lower heating value b) higher heating value	
H-OH	c) the standard heat of formation d) none of the above. d) none of the above. $d_{1}$ solution of potassium dichromate in water contains 15% K <sub>2</sub> Cr <sub>2</sub> O <sub>7</sub> by weight. 1000	
H-COOH	(ix) A 'limiting reactant' is the one which decides the	ETEC
H-OOCCH	a) equilibrium conversion b) yield b) yield c) selectivity b) yield c) selectivity b) yield c) selectivity b) yield c) selectivity c) selectivity c	FIEC
пзоосспз	d) rate constant.	
n monoxide a	(x) In chemical process, the recycle stream is purged for	
stion 1	a) increasing the yield b) enriching the product b) enriching the product	
d in the m	d) energy conservation. d) energy conservation. 6+6=12	TADU
a in the reac	Group - R	VIARY
2 and No and	2.(a) Using Buckinghamine it	
ively.)	pump (Q) is given by: $\pi$ theorem, show that the volumetric discharge of a constinuously in a 1900 lit tank equipped with an agitator and withdrawing 10%	
to the reak	$O = ND^3 f \int_{a}^{BH} \mu$	
es of line in	Where N is the mean of Silver	apoga
rough the	g, the acceleration due to gravity a the	as far
ons the relation	and H the head of fluid	us jui
te the mole	(b) Over a short tame	
ition is 50 m	relationship given by:	
10g of	$\mu = 4 \exp \left( \frac{B}{B} \right)$ ii) the molar humidity of air if its temperature is reduced to 15°C and pressure is	
ter with all	Determine the values $race f(\overline{T})$ Determine the values $race f(\overline{T})$ Determine the values $race f(\overline{T})$ iii) the weight of water condensed per 100 m <sup>3</sup> of original wat air	
ndensed 4	T, (in K) 303 312 312 312 312 312 312 312 312 312 31	
d the net h	$\mu$ , (in mPa.S) 0.843 0.739 0.651 0.595 0.595 0.595 0.595	
atent heat o	0.365 0.524 Group - D	·e
ionina Bana	3.(a) Calculate the composition of the	
D Roltrig Q	containing 35% benzene, 40 % toluene and 25 %	
A yield o	pressures of benzene, toluene and o-xylene are respectively 1340 FCO = 12100 The fresh feed to an ammonia production process contains 24.75 mole % nitrogen	
and hoghin	(b) A vapour stream containing 65 mel 96 is combined with a recycle	
misodmor	with a liquid mixture of the same two species. The prese	
	absolute. Use Raoult's law to estimate the composition of the liquid For stronger in which essentially all of the ammonia is removed, and the remaining	
Market Shirts	(b) the vapour pressures (P <sup>0</sup> ) in mm Hg are given by the equations:	
288 AB22	$\log P_s = 7.06623 - \frac{1307.434}{T+214.985}$ and $\log P_t^0 = 6.95805 - \frac{1346.773}{1346.773}$ over must be taken off. The recycle stream contains 12.5 mole% inerts. Calculate the	
ad the file of	where, remperature (T) is in $\circ$ C $T+219.693'$ $T+219.693'$ to the ratio (moles purge gas/mole of gas leaving the	
	$6^{+1}$ (a) Pr	
	<sup>overall</sup> Conversion of program The every large time in a catalytic reactor for a 95%	
	CHEN 2104 2 2 $H_{\text{EN 2104}}$	
. The second sec	3	
The second day in the second		

CS/B.Tech/CHE/Odd/Sem-3rd/CH (CHE)-301/2015-16



## MAULANA ABUL KALAM AZAD UNIV WEST BENGA

## CH (CHE)-30

# BASIC ENVIRONMENTAL ENGINEERING A

Time Allotted: 3 Hours

1.

The questions are of equ The figures in the margin indic Candidates are required to give their answers in the All symbols are of usual si

### GROUP A (Multiple Choice Type

Answer any ten questions.

- (i) The catalysts used in the Three Way type catalyt (B) Pt + Pt
  - (A) Pt + Pd(C) Ru + Rh(D) Pt + Rt
- (ii) Which one of the following is true for waste wat
  - (A) BOD > COD(B) COD >(C) BOD = COD(D) BOD =
- (iii) Water will be considered saline if the TDS value
  - (A) < 1500 mg/L; (B) > 5000 (D) none o
  - (C) < 500 mg/L; (D)

### CS/B.Tech/CHE/Odd/Sem-3

10.(a) Calculate the standa  $C_2H_5OH(1) + C$ Heats of combustion  $C_2H_5OH$   $CH_3COOH$  $C_2H_5OOCCH_3$ 

- (b) Carbon monoxide a air at 500° C in 90 combustion leave evolved in the reac burned assuming co CO<sub>2</sub>, O<sub>2</sub> and N<sub>2</sub> ar respectively.)
- 11.(a) 50 moles of liquid leaks through the conditions the relati Calculate the mole composition is 50 m
  - (b) When 1.0g of n calorimeter, with al being condensed, 4 value and the net h C. The latent heat o

### B.TECH/CHE/3rd SEM /CHEN 2104/2015

from the reactor is separated into two streams: one, the product which  $c_{0h}$   $C_{3}H_{6}$ , and 0.555% of unreacted propane. The other contains the baland unreacted propane and 5% of the propylene formed and is recycled to the Calculate the composition of the product, the ratio (moles recycled)/(moles free and the single-pass conversion.

(b) Find the overall and single pass conversion of A according to the schen below:



8.(a) Calculate the heat required to bring 150 mol / hr of a stream containing  $_{00}$  and 40 % C<sub>3</sub>H<sub>8</sub> by volume from 0°C to 400°C.

[For  $C_2H_6$ ,  $C_P = 0.04937 + 13.92 \times 10^{-5} \text{ T} - 5.816 \times 10^{-8} \text{ T}^2 + 7.280 \times 10^{-12} \text{ T}^3$ For  $C_3H_8$ ,  $C_P = 0.06803 + 22.59 \times 10^{-5} \text{ T} - 13.11 \times 10^{-8} \text{ T}^2 + 31.71 \times 10^{-12} \text{ T}^3$ Where,  $C_P$  is in kJ / mol. °C and T = temperature in °C ]

(c) The standard heats of the following combustions reactions have been determine the heat of formation of ethane.  $C_2H_6 + 7/2 \ 0_2 \rightarrow 2CO_2 + 3H_2O$   $\Delta H_1 = -1559.8 \text{ kJ / mol};$   $C + O_2 \rightarrow CO_2$   $\Delta H_2 = -393.5 \text{ kJ / mol};$  $H_2 + 1/2 \ 0_2 \rightarrow H_2O$   $\Delta H_3 = -285.8 \text{ kJ / mol}.$ 

9.(a) Calculate the theoretical flame temperature of a gas containing 20% CO and when burned with 100% excess air, both air and gas initially being at 25°C. [Heat capacity ( $C_P$ ) = a + b T + c T<sup>2</sup>, Kcal / kmol. K]

The values of the coefficients for different materials are as follows:

Material	a	b x 10 <sup>3</sup>	c x 10 <sup>6</sup>
CO2	6.339	10.14	- 3.415
02	6.117	3.167	- 1.005
N <sub>2</sub>	6.457	1.389	- 0.069

The standard heat of formation of  $CO_2 (\Delta H^{0}_{298K}) = -67636$  kcal /mol

(b) A well stirred batch reactor wrapped in an electrical heating mantle is charged liquid reaction mixture. The reactant must be heated from an initial temperar 25°C to 250°C before the reaction can take place at a measurable rate. Using the given below determine the time required for this heating to take place. Reactant: mass = 1.5 Kg,  $C_V = 0.90$  Kcal / Kg. °C; Reactor: mass = 3.0 Kg,  $C_V = 0.7$  Kg. °C; Heating rate(Q) = 500 W; [Negligible reaction and no phase change heating. Negligible energy added to the system by the stirrer].